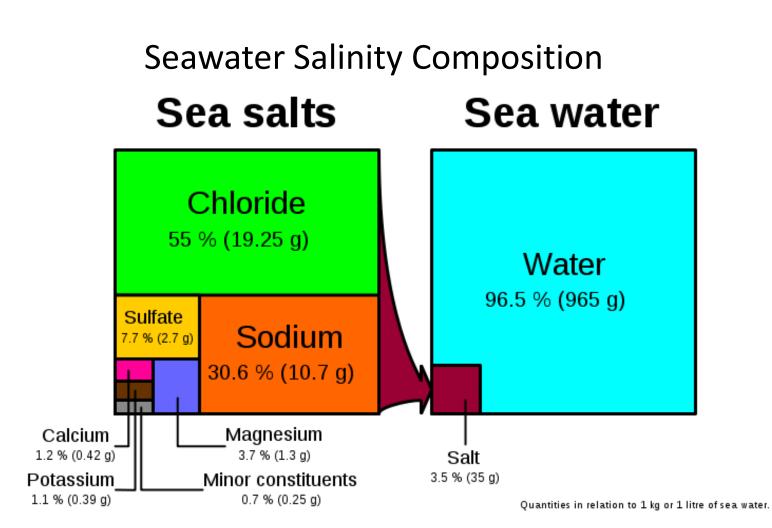
#### GE Power & Water Water & Process Technologies

# Innovative water treatment solutions for seawater open evaporative systems

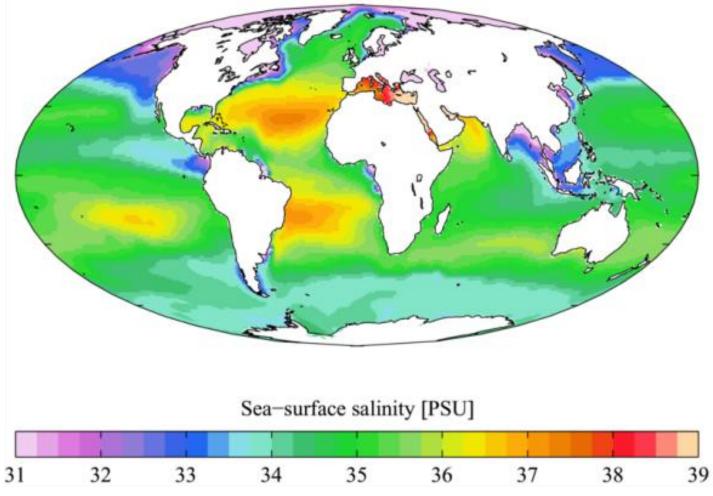
#### 1st NACE Jubail Industrial Forum 17 – 19 Oct, 2011

#### Shereif Alsayed

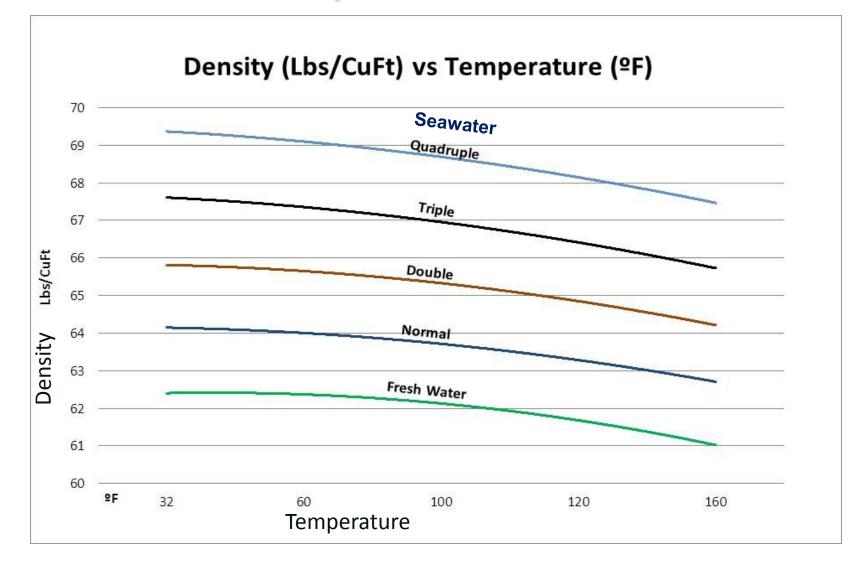


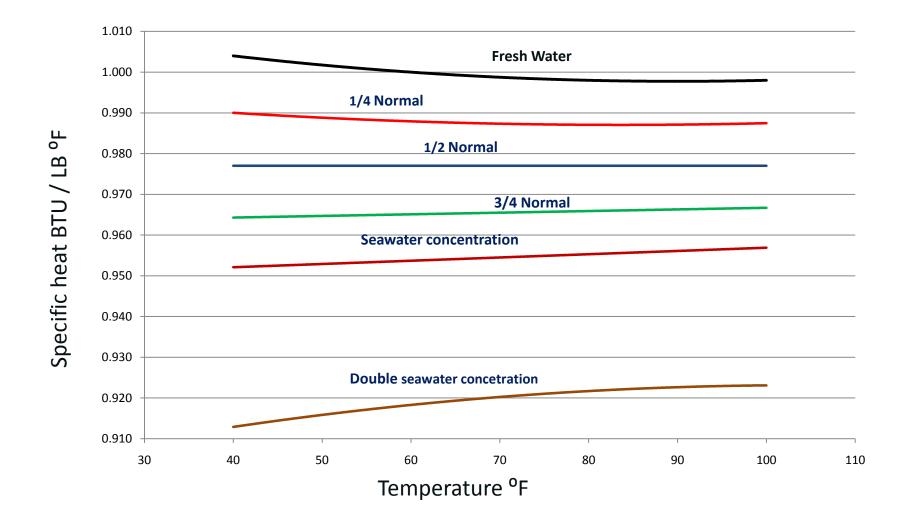


Seawater Salinity Distribution



Source: World Ocean Atlas 2005. Retrieved 17 October 2010





#### Factors affecting physical properties **Density Specific** Heat

#### PARAMETER

- Conductivity
- Temp
- Depth
- Desalination plants reject.
- Vicinity of other plants.

•Effect of lower specific heat

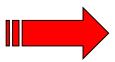
Energy required = heat rejected= Q

Q = specific heat x mass x DT

Q(brackish water) = specific heat x mass x DT

Q(Seawater) = specific heat x mass x DT

Q brackish water / Q seawater = > 1



Brackish cooling system is less efficient Q: Cal ,C<sub>p</sub>: Cal/g °C, Mass:g, DT: °C Q: BTU, C<sub>p</sub>: Btu/ Lb °F, Mass: Lb, DT: °F

•Effect of higher density

Energy required = heat rejected= Q

Q = specific heat x mass x DT

Q(brackish water) = specific heat x mass x DT

Q(Seawater) = specific heat x mass x DT

Q brackish water / Q seawater = < 1

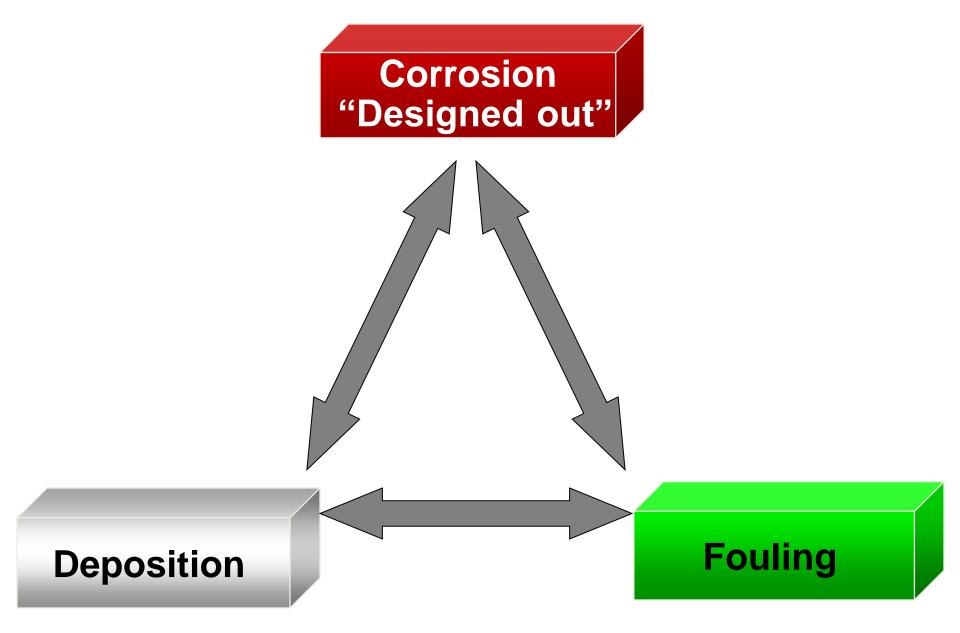
Seawater cooling system is less efficient Q: Cal ,C<sub>p</sub>: Cal/g °C, Mass:g, DT: °C Q: BTU, C<sub>p</sub>: Btu/ Lb °F, Mass: Lb, DT: °F

Loss in energy can be compensated by:

- Increased tower size.
- □ Adjusting fan horsepower.
- □ Increased circulation rate.

#### **Treatment Concerns**





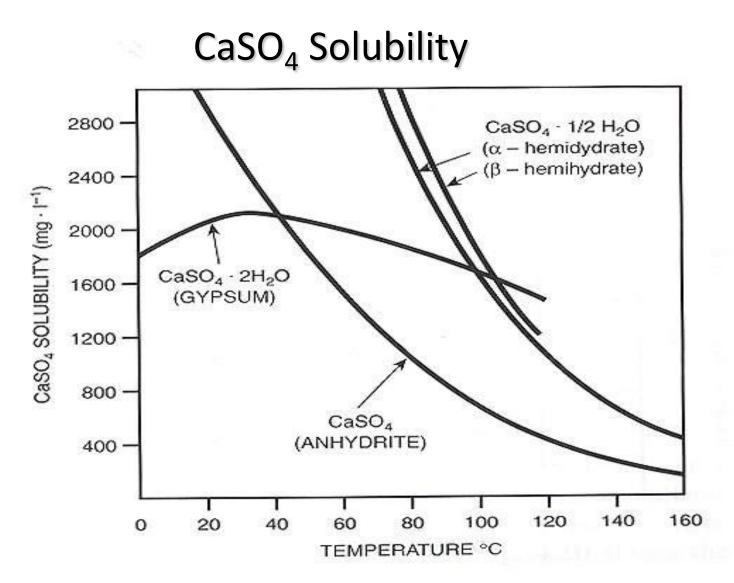


**Calcium Carbonate** 

- Scale potential depends on:
- Calcium
- D pH control
- Alkalinity
- Temperature
- Ionic strengths

**Calcium Sulphate** 

- Scale potential depends on:
- Calcium
- Sulphate
- Ionic strength



#### Silicate

#### Factors affecting deposition

- Magnesium
- Silicate
- 🛛 pH

#### **New Technology**



#### **Treatment practices overview**

- $\Box$  Typical cycles (1.2 1.3).
- □ No pH control or adjustment.
- □ Continuous chlorination.
- □ Material of construction.
  - Sacrificial anode for yellow metallurgy alloys.

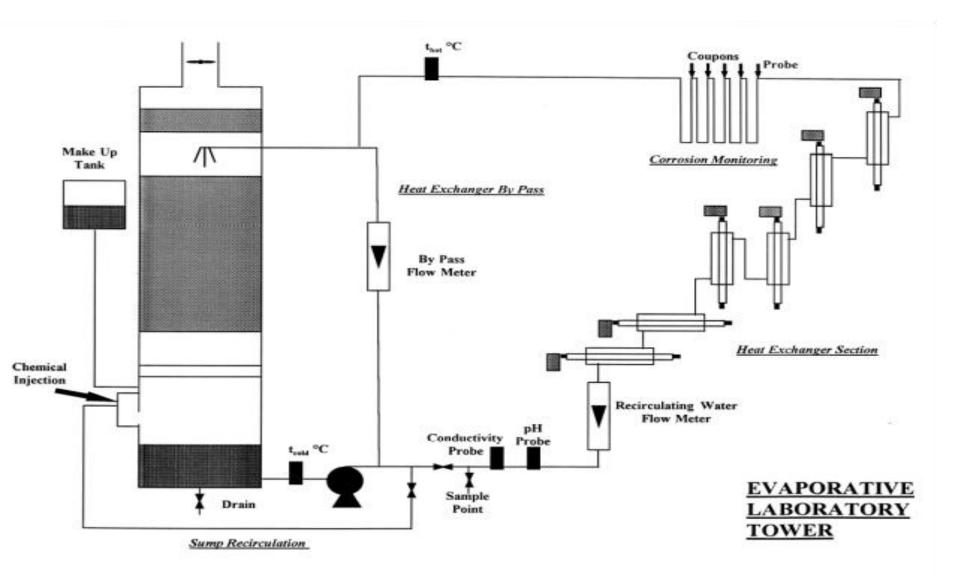
#### Sea Water and Open Evaporative Cooling



SALT WATER By John A. Nelson • The Marley Cooline v • November 5, 1986

GE technology reached > 80,000 ppm, free pH **Intrated to approximately 55,000 ppm** "Generally, sea water salinity with pr m without serious scaling problems in the centrations are possible but pH control by acid exchape probably be required. Two of the major users of sea addit mg towers operate to 55,000 ppm salinity as the upper limit and water this procedure has been satisfactory."

#### **Evaluation of Inhibitors**



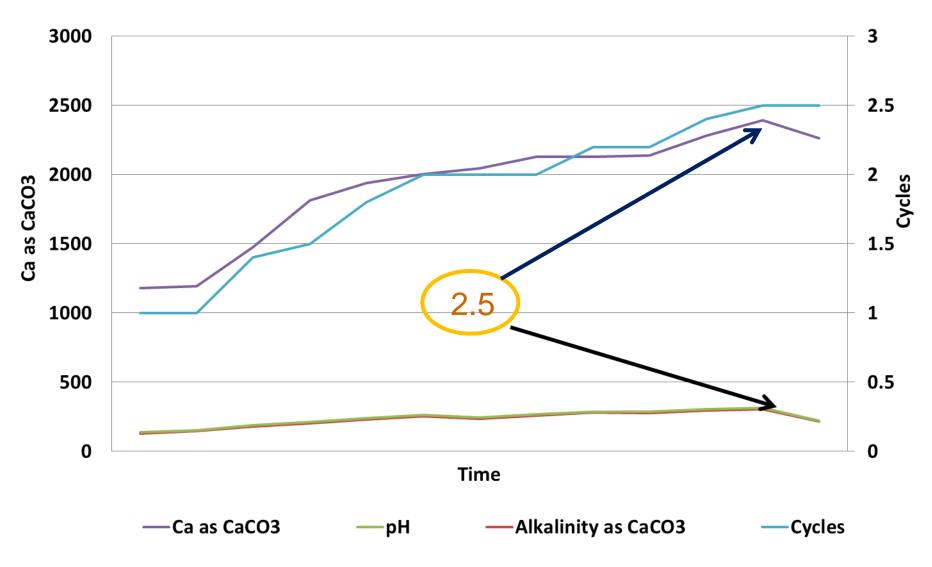
### **Operating Conditions**

- Coupons: Ti , 70/30 Cu/Ni,
- CRM Probe:

70/30 Cu/Ni

- Heat Exchanger Tubes: Ti, 70/30 Cu/Ni
- Water Temperature: 40 °C
- Estimated Skin Temperature: 52 °C
- Water Velocity: 1.5 m/s

#### pH, Alkalinity , Ca .vs. Cycles



#### **Corrosion Coupons**



#### CRM probe corrosion Cu/ Ni 70-30 : 0.9 mpy

#### Heat exchanger tubes



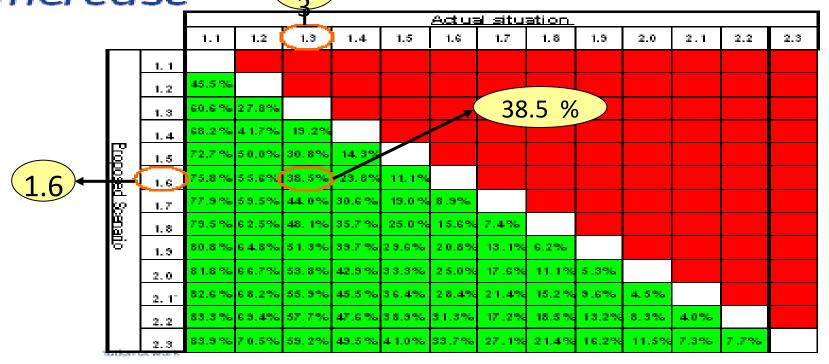


### **Technology** Guide

- □ Stiff & Davis Max 1.50 @ 52°C (skin)
- □ Up to theoretical LSI of 2.5 @ 52ºC.
- □ Max 2.4 cycles (depending on chemistry).
- **Free pH**, pH of 8.4.



## % Make-up Reduction by Cycles



- □ 38.5 % saving in make up requirement.
- Reduced energy consumption (make up, blow down pumps)
- □ Forgiving program, higher tolerance for upsets and excursions.
- □ Compatible with halogenation practices.

#### **Technology Features & Advantages**

